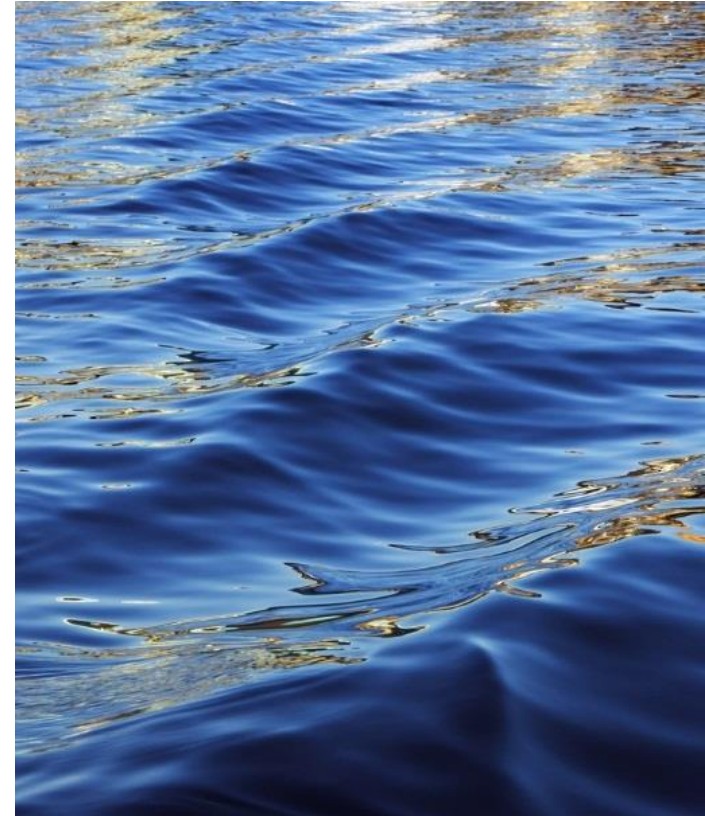




# Water supply and sanitation systems

Lecturer: Eng. Tawfiq Saleh  
Fall 2024/2025



# Chapter 1: Introduction

## Main principles of Environment Engineering

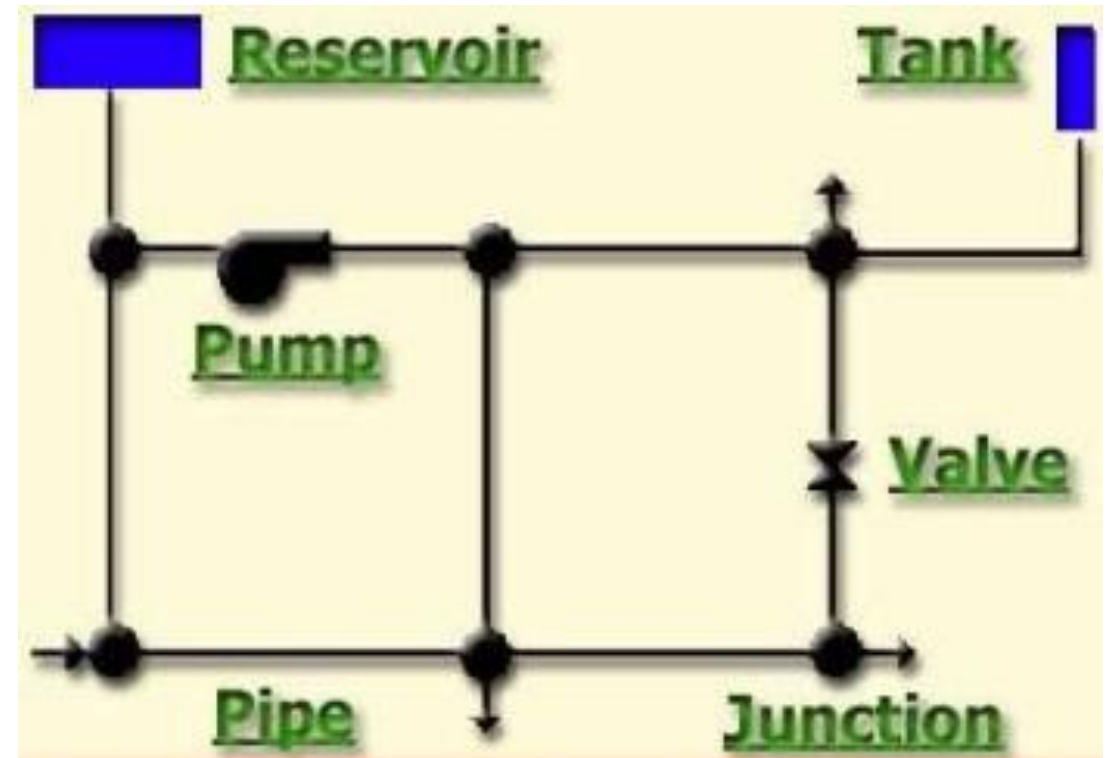
- Provision of safe, tasty and sufficient public water supply.
- Proper handling, disposal or recycling of wastewater and solid waste.
- Control of water, soil, atmospheric pollution and noise pollution.

# Water Distribution Networks (WDNs)

A water distribution network (WDN) is comprised of a number of links (mainly pipes) connected together (at nodes) to form loops and/or branches

The links represent in general pipes, pumps, fittings, valves, etc.

Loops: closed circuits that consist of a series of links in which the nodes are supplied from more than one pipe

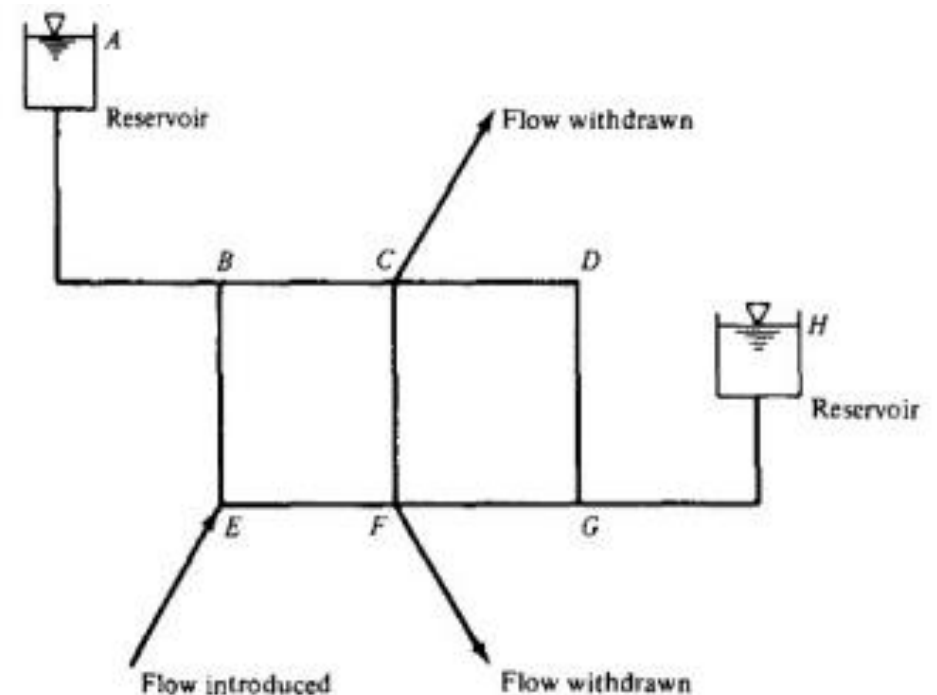


# Water Distribution Networks (WDNs)

Nodes: They are the end edges of the pipes where two or more pipes are joined.

Water can enter or leave the network at these nodes.

The reservoirs are considered fixed-head nodes where the head can be assumed constant.



# What is the Analysis of WDNs?

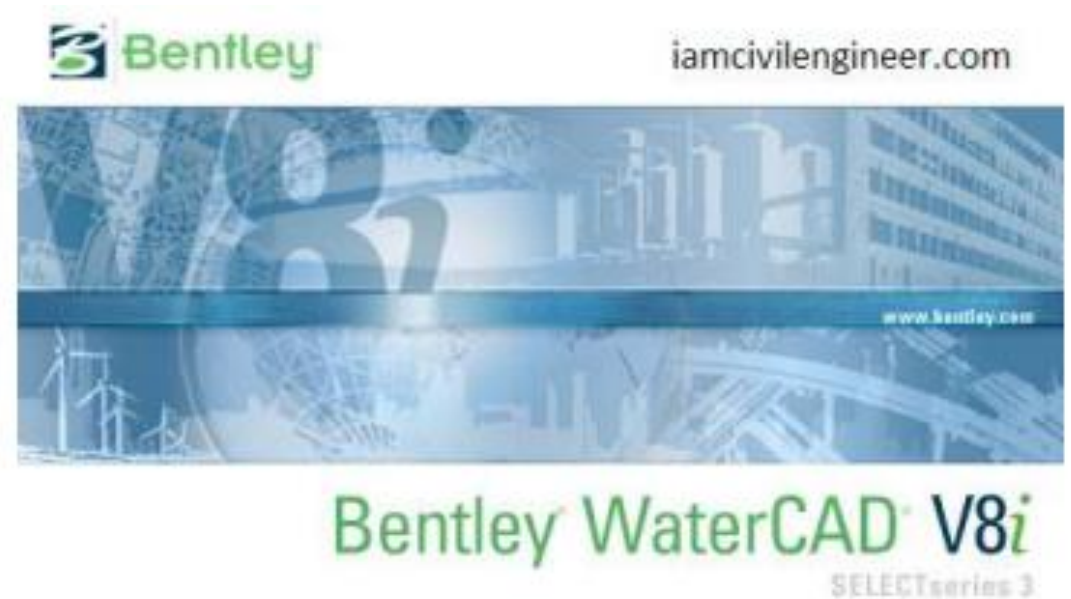
Analysis of WDNs implies obtaining the following:

- o **Water velocities in pipes**
- o **Water pressure at nodes.**

Network analysis is called simulation.

There are several methods to solve the network equations among which is for instance Hardy Cross Method.

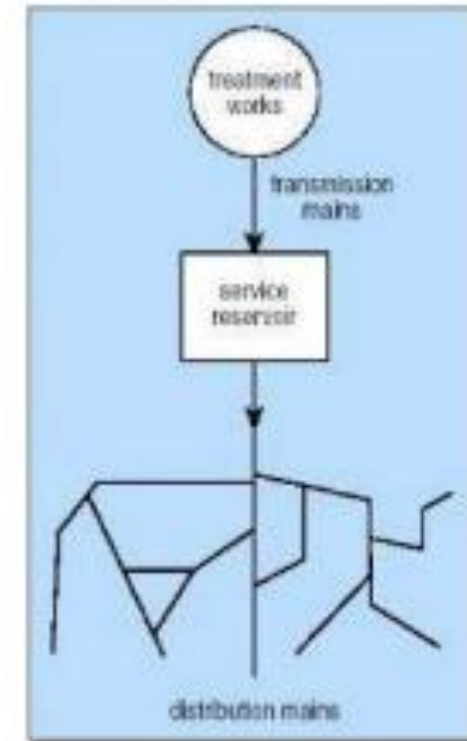
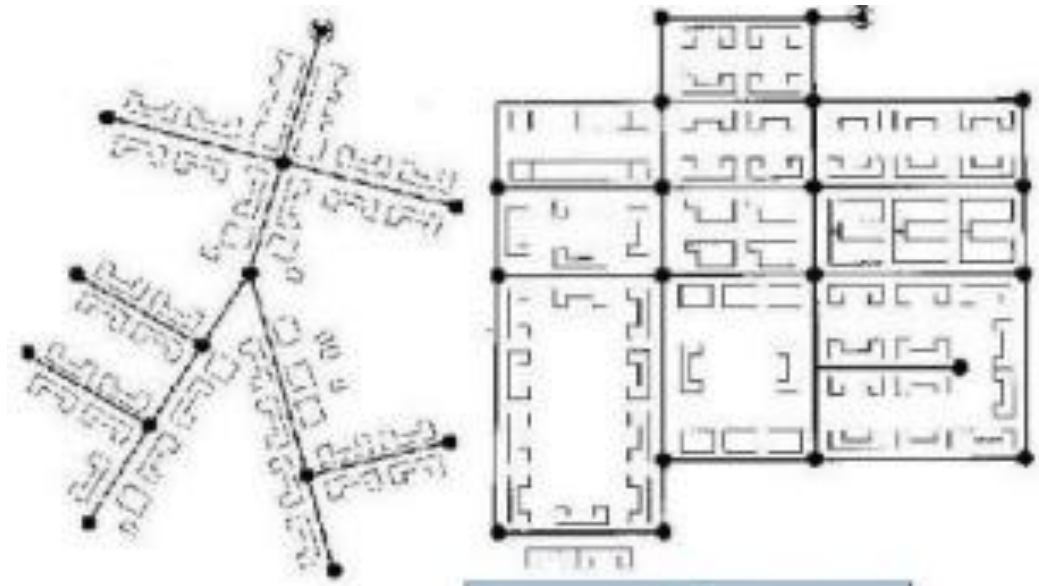
For large number of pipes and nodes, solving these equations manually becomes impractical and unfeasible For that, network simulation (modeling) packages exists such as WaterCAD



# Types of WDNs

WDNs may be classified as looped systems, branching systems, or a combination of the two.

The configuration of the system is influenced by street patterns.



# What does a node represent in reality?



# What does a reservoir represent in reality?





# Water pipes



# Water valves

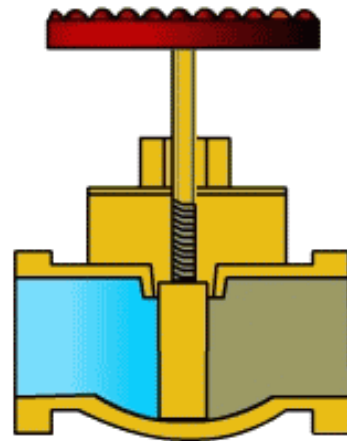


## Types of Water Valves

# Gate Valves

Gate valves are used to throttle flow ( reduce, regulate, turn off )

Gate valves function predominantly to isolate a pipe section; a valve block will be installed on an intersection between the pipes. Consequently, these valves normally operate in an open/closed position. Flow regulation is possible but is not common; the disk that is partly exposed to the flow may eventually loosen, causing leakage when it is in the closed position.



Gate Valve Closed

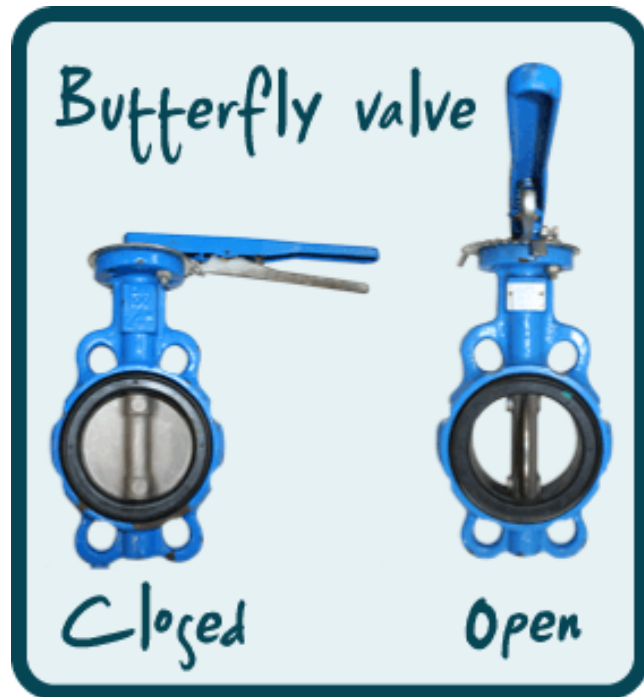


Gate Valve Opened

# Butterfly Valves

(Butterfly valves are used to turn off the flow)

Butterfly valves are widely used in pumping stations as they are compact in size, and easier to operate and cheaper than comparable gate valves

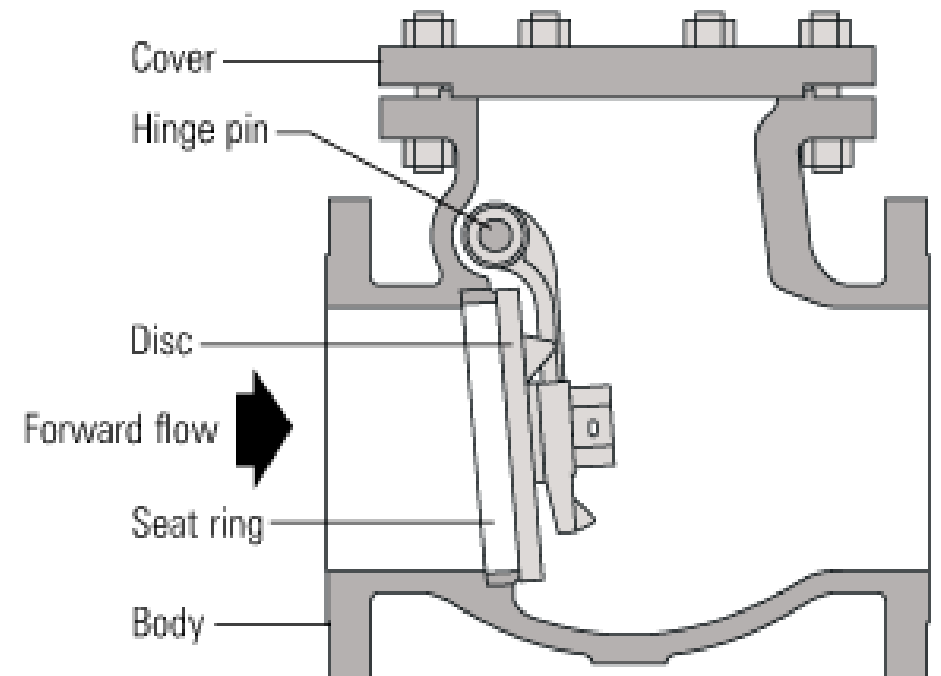


# Check Valves

Check valves: or One way valves are used to maintain flow in one direction. An opposite flow direction causes the valve to close and remain closed until the flow is re-established in its original direction. There are two types: ball valves and swing gate valves

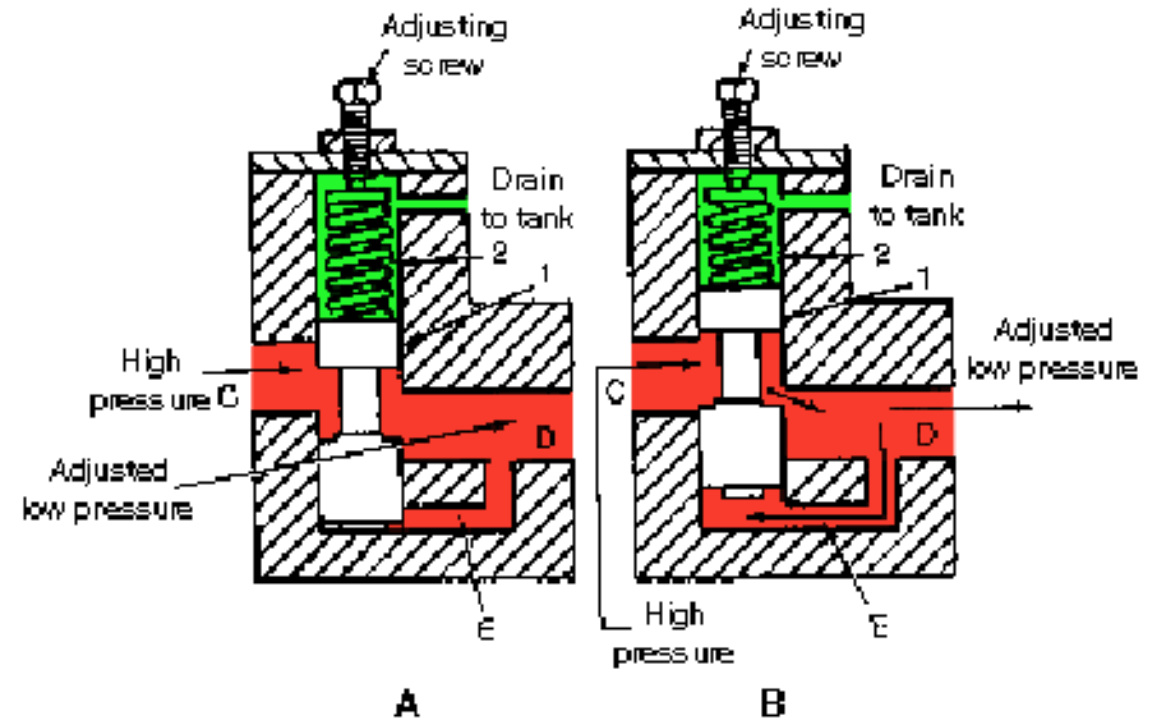
Check valve working animation:

[https://youtu.be/RZZjNv1EgGo?si=NR\\_g7u1E7\\_ggVuVE](https://youtu.be/RZZjNv1EgGo?si=NR_g7u1E7_ggVuVE)



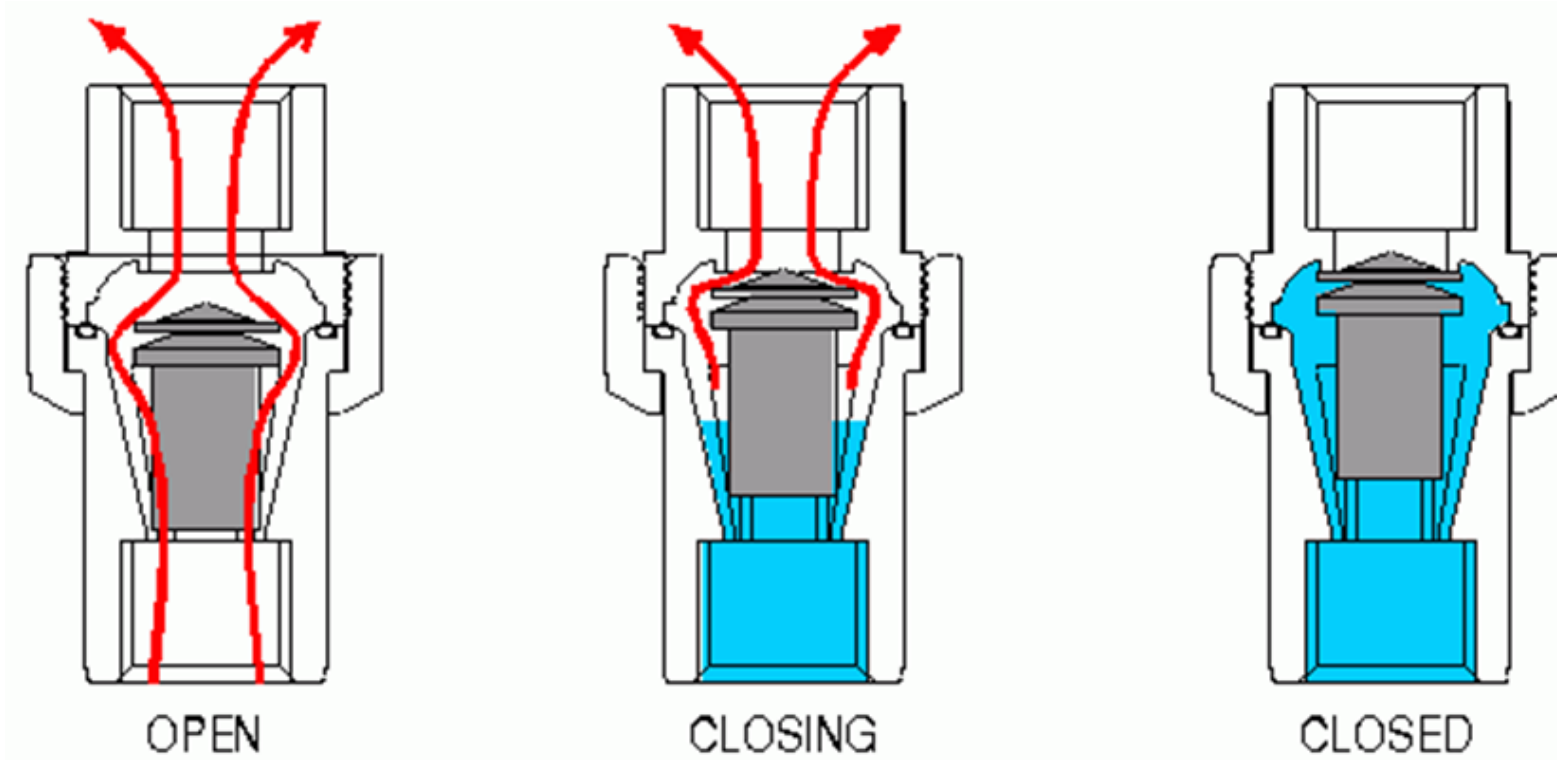
# Pressure Reducing Valves

PRV are normally used to control the pressure in isolated parts of networks if it becomes too high. When the pressure upstream of the valve rises above the pre-set value, the valve will start closing until the downstream pressure is equal to the pre-set pressure. If the upstream pressure is below the pre-set value, the valve operates fully opened

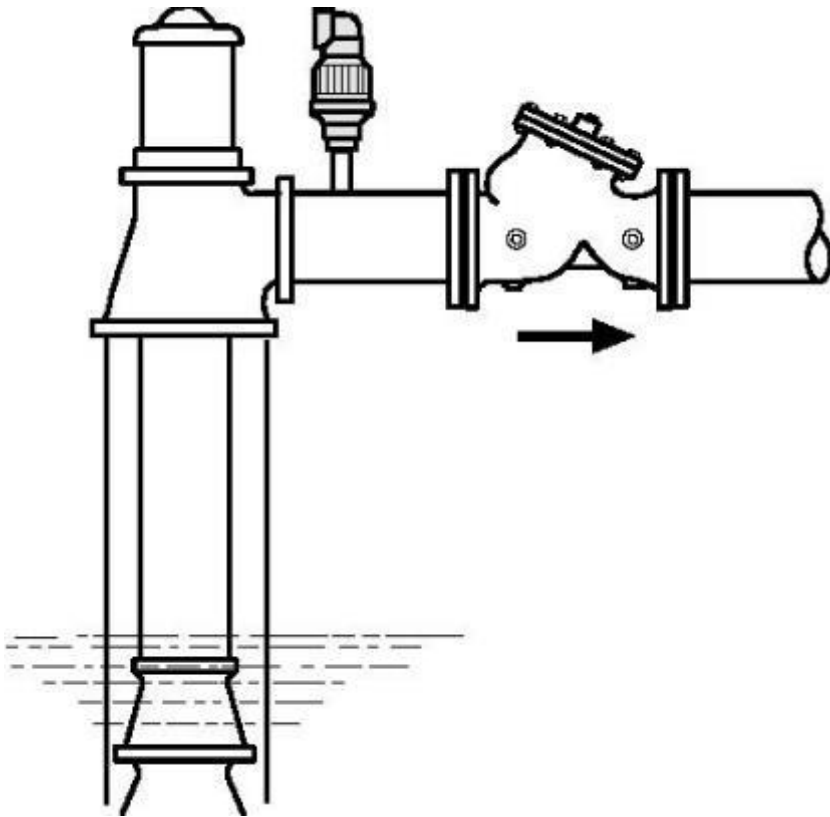


# Air Release Valve

is a special type of valve that helps to release air from pipelines, which prevents reduction of the conveying capacity.



# Air Release Valve

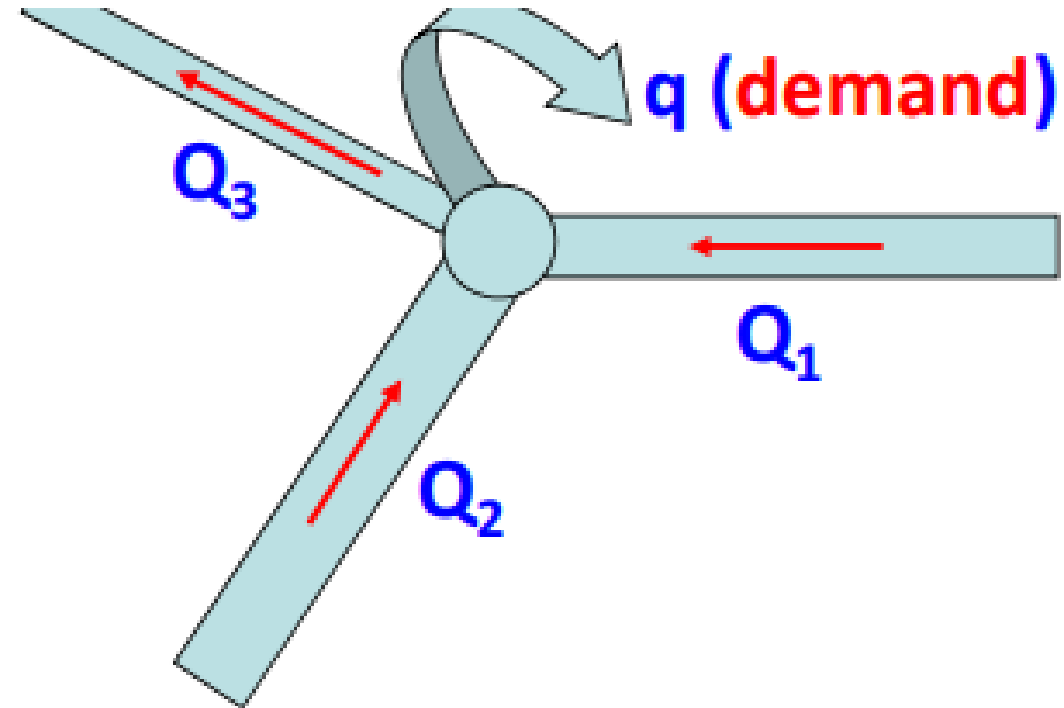




# Main Principles of WDN Analysis

**Continuity:** The algebraic sum of the flow rates in the pipes meeting at a node together with any external flows is zero.

$$Q_1 + Q_2 = Q_3 + q$$



# Main Principles of WDN Analysis

**Energy conservation**: For all paths around closed loops, the accumulated energy loss including minor losses minus any energy gain or heads generated by pumps must be zero

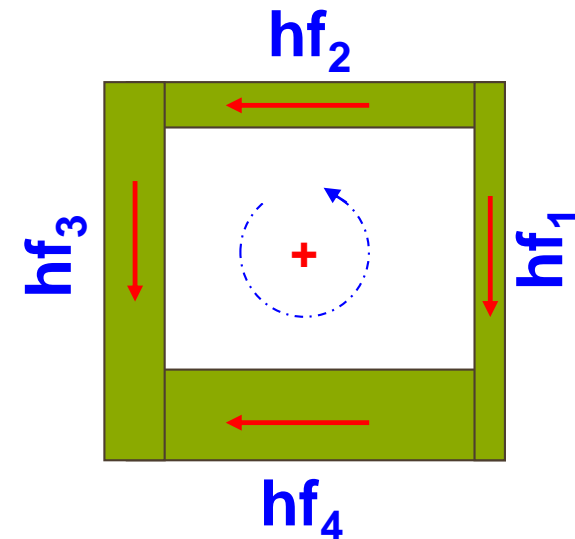
A part of a looped network

Closed loop

Given total headloss for each link (pipe) as  $h_f$

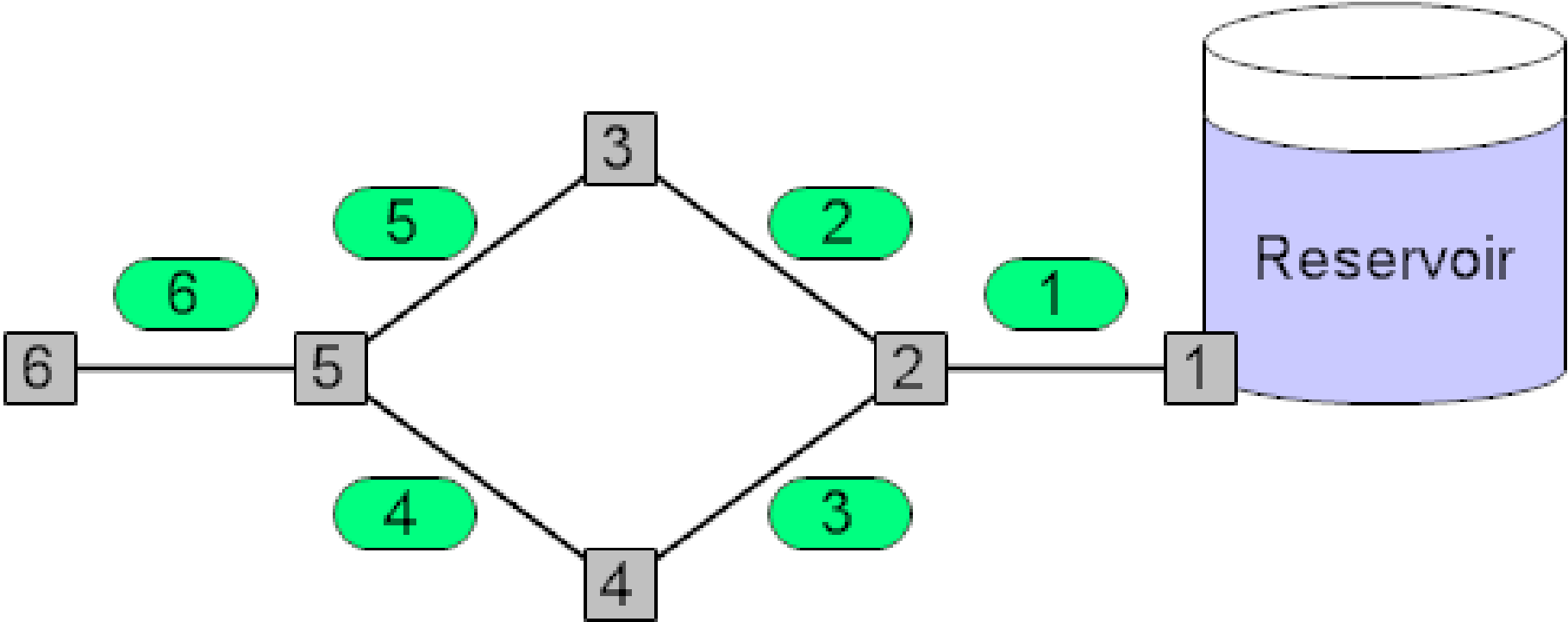
Assume counterclockwise to be positive

$$-hf_1 - hf_4 + hf_3 + hf_2 = 0$$



# Example 1

Write the *continuity* and *energy conservation* equations for the following network:

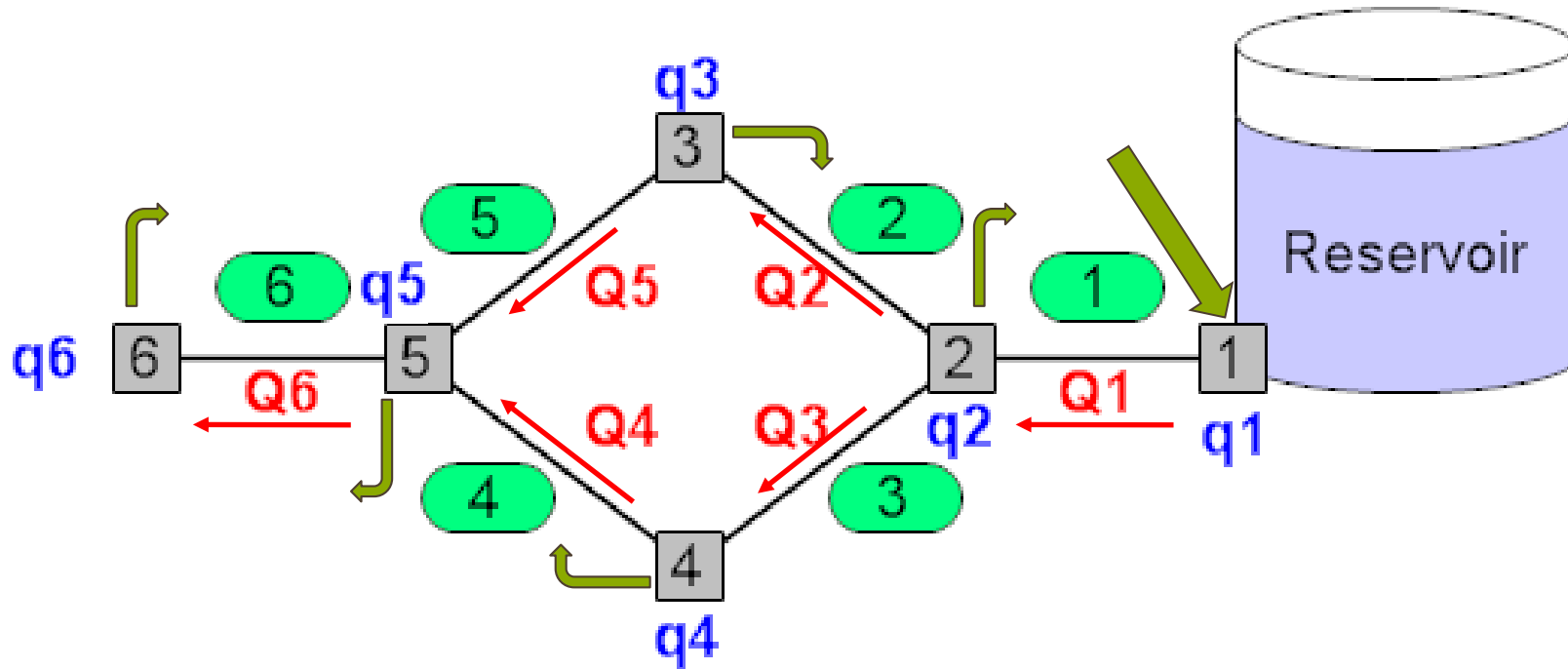


# Example 1

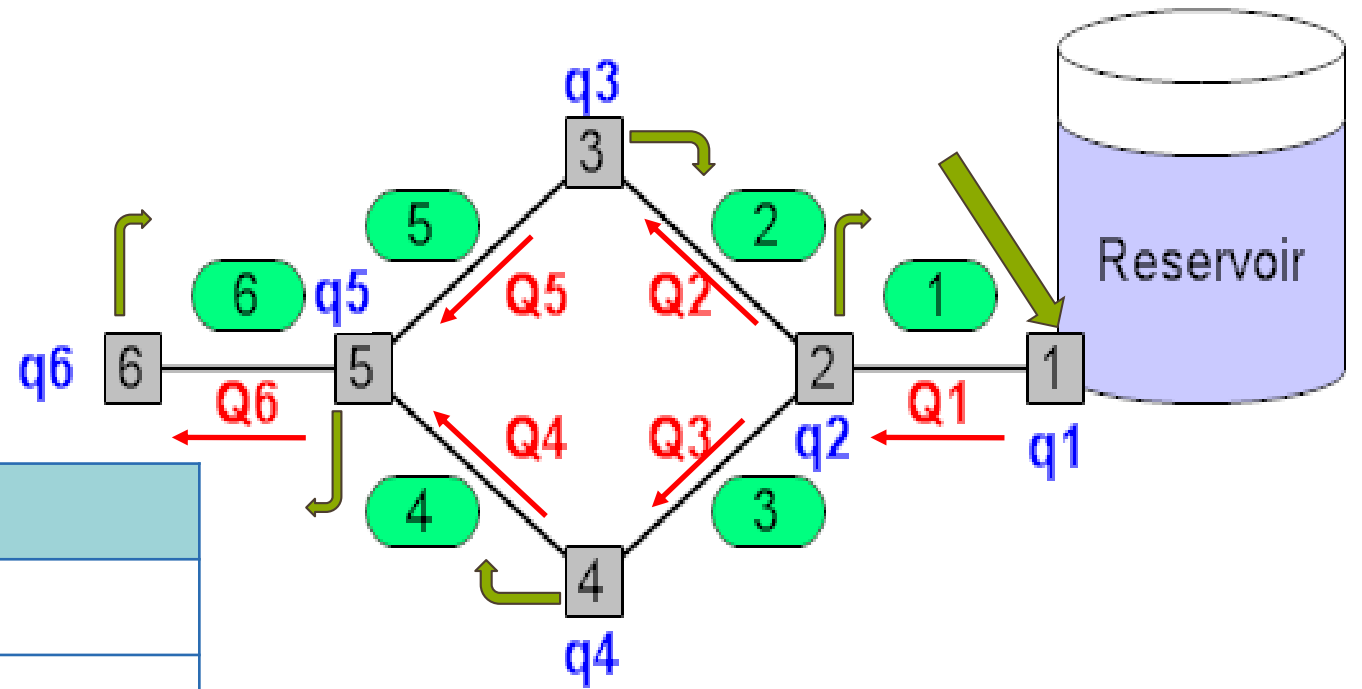
- First of all, keep in mind two issues:
  - Nodes provide water or receive water
  - Links (pipes) convey water to nodes or from nodes
- General input data includes:
  - Ground surface elevation ( $z$ )
  - Nodal demand or supply ( $q$ )
  - Total head at the source
  - Pipe diameter ( $D$ )
  - Pipe length ( $L$ )
  - Hazen-Williams coefficients

# Example 1

- Label the nodal demands and pipe flows in the figure and assume flow directions
- This is necessary to be able to formulate the equations needed to analyze the network



# Example 1



| <b>Node ID</b> | <b>Continuity</b>               |
|----------------|---------------------------------|
| 1              | $Q_1 = q_1$                     |
| 2              | $Q_1 = Q_2 + Q_3 + q_2$         |
| 3              | $Q_2 = q_3 + Q_5$               |
| 4              | $Q_3 = q_4 + Q_4$               |
| 5              | $Q_4 + Q_5 = q_5 + Q_6$         |
| 6              | $Q_6 = q_6$                     |
| <b>Loop</b>    | <b>Energy Conservation</b>      |
| 2 – 5 – 4 – 3  | $hf_2 + hf_5 - hf_4 - hf_3 = 0$ |

# Hydraulics review

## Reynolds Number

$$Re = \frac{\rho V_{avg} D}{\mu} = \frac{V_{avg} D}{\nu}$$

$V_{avg}$ : average flow velocity (m/s)

$D$ : diameter in the case of pipes (m)

$\mu$ : dynamic viscosity (kg/m.s)

$\nu$ : kinematic viscosity (m<sup>2</sup> /s)

$\rho$ : density (kg/m<sup>3</sup> )

**$Re \leq 2,000$  Laminar**

**$2,000 \leq Re \leq 4,000$  Transitional**

**$Re \geq 4,000$  Turbulent**

## Density of Liquid Water From 0°C to 100°C

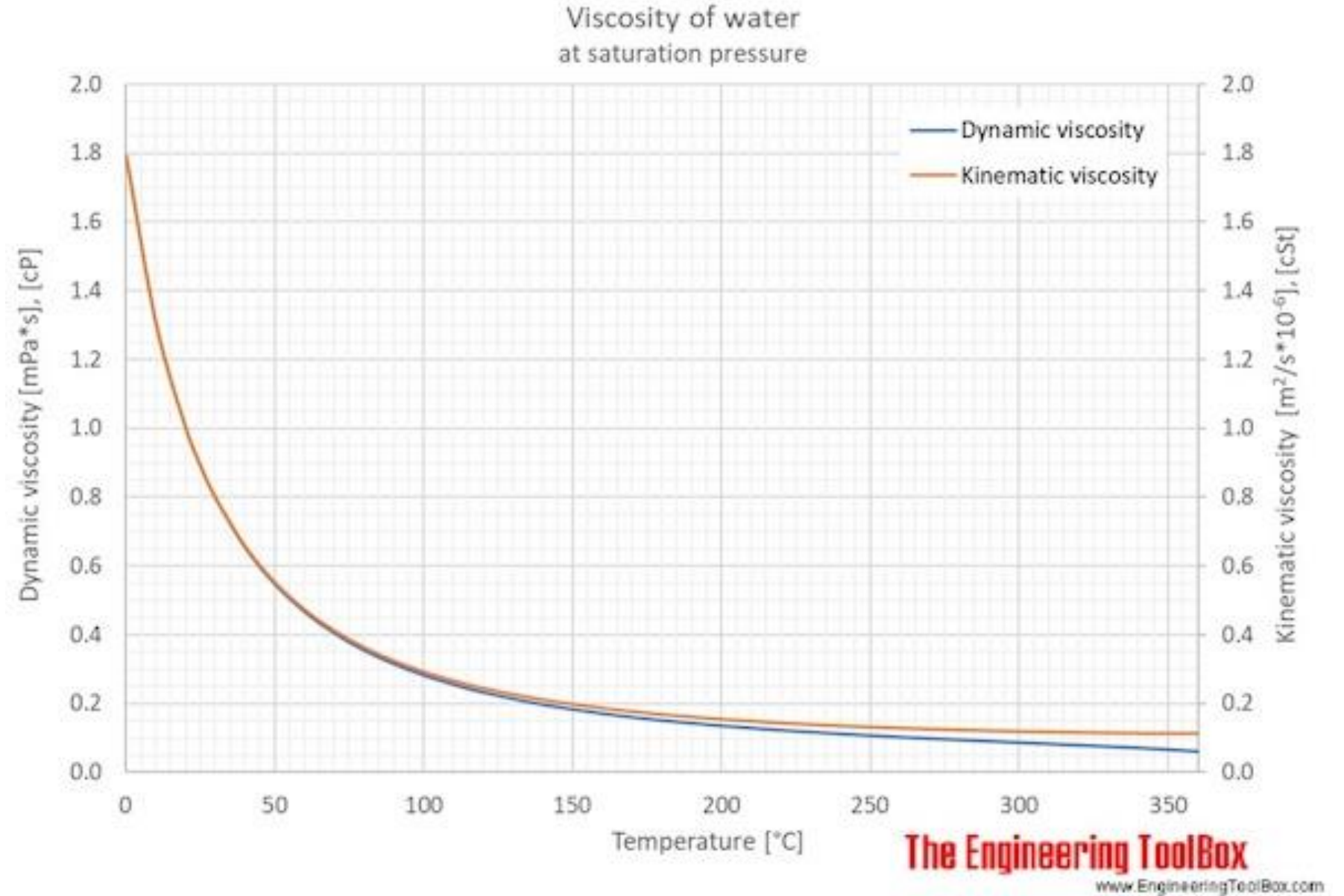
External pressure: 1 atm = 101 325 Pa

| Temperature °C | Density kg/m <sup>3</sup> | Temperature °C | Density kg/m <sup>3</sup> | Temperature °C | Density kg/m <sup>3</sup> |
|----------------|---------------------------|----------------|---------------------------|----------------|---------------------------|
| 0 (ice)        | 917.00                    | 33             | 994.76                    | 67             | 979.34                    |
| 0              | 999.82                    | 34             | 994.43                    | 68             | 978.78                    |
| 1              | 999.89                    | 35             | 994.08                    | 69             | 978.21                    |
| 2              | 999.94                    | 36             | 993.73                    | 70             | 977.63                    |
| 3              | 999.98                    | 37             | 993.37                    | 71             | 977.05                    |
| 4              | 1000.00                   | 38             | 993.00                    | 72             | 976.47                    |
| 5              | 1000.00                   | 39             | 992.63                    | 73             | 975.88                    |
| 6              | 999.99                    | 40             | 992.25                    | 74             | 975.28                    |
| 7              | 999.96                    | 41             | 991.86                    | 75             | 974.68                    |
| 8              | 999.91                    | 42             | 991.46                    | 76             | 974.08                    |
| 9              | 999.85                    | 43             | 991.05                    | 77             | 973.46                    |
| 10             | 999.77                    | 44             | 990.64                    | 78             | 972.85                    |
| 11             | 999.68                    | 45             | 990.22                    | 79             | 972.23                    |
| 12             | 999.58                    | 46             | 989.80                    | 80             | 971.60                    |
| 13             | 999.46                    | 47             | 989.36                    | 81             | 970.97                    |
| 14             | 999.33                    | 48             | 988.92                    | 82             | 970.33                    |
| 15             | 999.19                    | 49             | 988.47                    | 83             | 969.69                    |
| 16             | 999.03                    | 50             | 988.02                    | 84             | 969.04                    |
| 17             | 998.86                    | 51             | 987.56                    | 85             | 968.39                    |
| 18             | 998.68                    | 52             | 987.09                    | 86             | 967.73                    |
| 19             | 998.49                    | 53             | 986.62                    | 87             | 967.07                    |
| 20             | 998.29                    | 54             | 986.14                    | 88             | 966.41                    |
| 21             | 998.08                    | 55             | 985.65                    | 89             | 965.74                    |
| 22             | 997.86                    | 56             | 985.16                    | 90             | 965.06                    |
| 23             | 997.62                    | 57             | 984.66                    | 91             | 964.38                    |
| 24             | 997.38                    | 58             | 984.16                    | 92             | 963.70                    |
| 25             | 997.13                    | 59             | 983.64                    | 93             | 963.01                    |
| 26             | 996.86                    | 60             | 983.13                    | 94             | 962.31                    |
| 27             | 996.59                    | 61             | 982.60                    | 95             | 961.62                    |
| 28             | 996.31                    | 62             | 982.07                    | 96             | 960.91                    |
| 29             | 996.02                    | 63             | 981.54                    | 97             | 960.20                    |
| 30             | 995.71                    | 64             | 981.00                    | 98             | 959.49                    |
| 31             | 995.41                    | 65             | 980.45                    | 99             | 958.78                    |
| 32             | 995.09                    | 66             | 979.90                    | 100            | 958.05                    |

$\rho$ : density (kg/m<sup>3</sup>)



$\mu$ : dynamic viscosity (kg/m.s)  
 $\nu$ : kinematic viscosity (m<sup>2</sup> /s)



## Example2

Determine whether the flow is laminar or turbulent if water at 70°C flows in a 1-in pipe with a flow rate of 285 L/min

$$Re = \frac{\rho V_{avg} D}{\mu} = \frac{V_{avg} D}{\nu}$$

# Example 2

$\nu$ : kinematic viscosity ( $m^2/s$ ) from the chart =  $0.42 \times 10^{-6}$

$D = 1 \text{ in} = 0.0254 \text{ m}$

$$V = \frac{Q}{A} = \frac{0.0475 \text{ m}^3/\text{sec}}{5.067 \times 10^{-4}} = 9.37 \text{ m/s}$$

$$Re = \frac{9.37 \frac{m}{s} \times 0.0254 \text{ m}}{0.42 \times 10^{-6} \text{ m}^2/\text{s}} = 566662$$

Then the flow is turbulent

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Then the flow is turbulent

# Hazen Williams for frictional head loss

$$h_f = 162.5 \times \left( \frac{Q}{C_{hw}} \right)^{1.852} \times D^{-4.87} \times L$$

Q in  $\left( \frac{m^3}{h} \right)$

D in (in).

$C_{hw}$  = Hazen Williams friction coefficient,

L = pipeline length in (m)

$h_f$  = frictional head loss (m).

**The Hazen-Williams coefficient ( $C_{hw}$ ) is usually taken as 140-150 for plastic and new steel pipes as shown in the following table.**

| Material                           | Hazen-Williams Coefficient | Material                                      | Hazen-Williams Coefficient |
|------------------------------------|----------------------------|---|----------------------------|
| ABS - Acrylonite Butadiene Styrene | 130                        | Ductile Iron Pipe (DIP)                       | 140                        |
| Aluminum                           | 130 - 150                  | Ductile Iron, cement lined                    | 120                        |
| Asbestos Cement                    | 140                        | Fiber   | 140                        |
| Asphalt Lining                     | 130 - 140                  | Fiber Glass Pipe – FRP                        | 150                        |
| Brass                              | 130 - 140                  | Galvanized iron                               | 120                        |
| Brick sewer                        | 90 - 100                   | Glass   | 130                        |
| Cast-Iron - new unlined (CIP)      | 130                        | Lead  | 130 - 140                  |
| Cast-Iron 10 years old             | 107 - 113                  | Metal Pipes - Very to extremely smooth        | 130 - 140                  |
| Cast-Iron 20 years old             | 89 - 100                   | Plastic                                       | 130 - 150                  |
| Cast-Iron 30 years old             | 75 - 90                    | Polyethylene, PE, PEH                         | 140                        |
| Cast-Iron 40 years old             | 64-83                      | Polyvinyl chloride, PVC, CPVC                 | 150                        |
| Cast-Iron, asphalt coated          | 100                        | Smooth Pipes                                  | 140                        |
| Cast-Iron, cement lined            | 140                        | Steel new unlined                             | 140 - 150                  |
| Cast-Iron, bituminous lined        | 140                        | Steel, corrugated                             | 60                         |
| Cast-Iron, sea-coated              | 120                        | Steel, welded and seamless                    | 100                        |
| Cast-Iron, wrought plain           | 100                        | Steel, interior riveted, no projecting rivets | 110                        |
| Cement lining                      | 130 - 140                  | Steel, projecting girth and horizontal rivets | 100                        |
| Concrete                           | 100 - 140                  | Steel, vitrified, spiral-riveted              | 90 - 110                   |
| Concrete lined, steel forms        | 140                        | Steel, welded and seamless                    | 100                        |
| Concrete lined, wooden forms       | 120                        | Tin   | 130                        |
| Concrete, old                      | 100 - 110                  | Vitrified Clay                                | 110                        |
| Copper                             | 130 - 140                  | Wrought iron, plain                           | 100                        |
| Corrugated Metal                   | 60                         | Wooden or Masonry Pipe – Smooth               | 120                        |
|                                    |                            | Wood Stave                                    | 110 - 120                  |

# Darcy-Weisbach Equation

$$h_f = f \frac{L V^2}{D 2g}$$

Darcy Friction Factor,  $f$

Duct Length,  $L$  (m)

Duct Diameter,  $D$  (m)

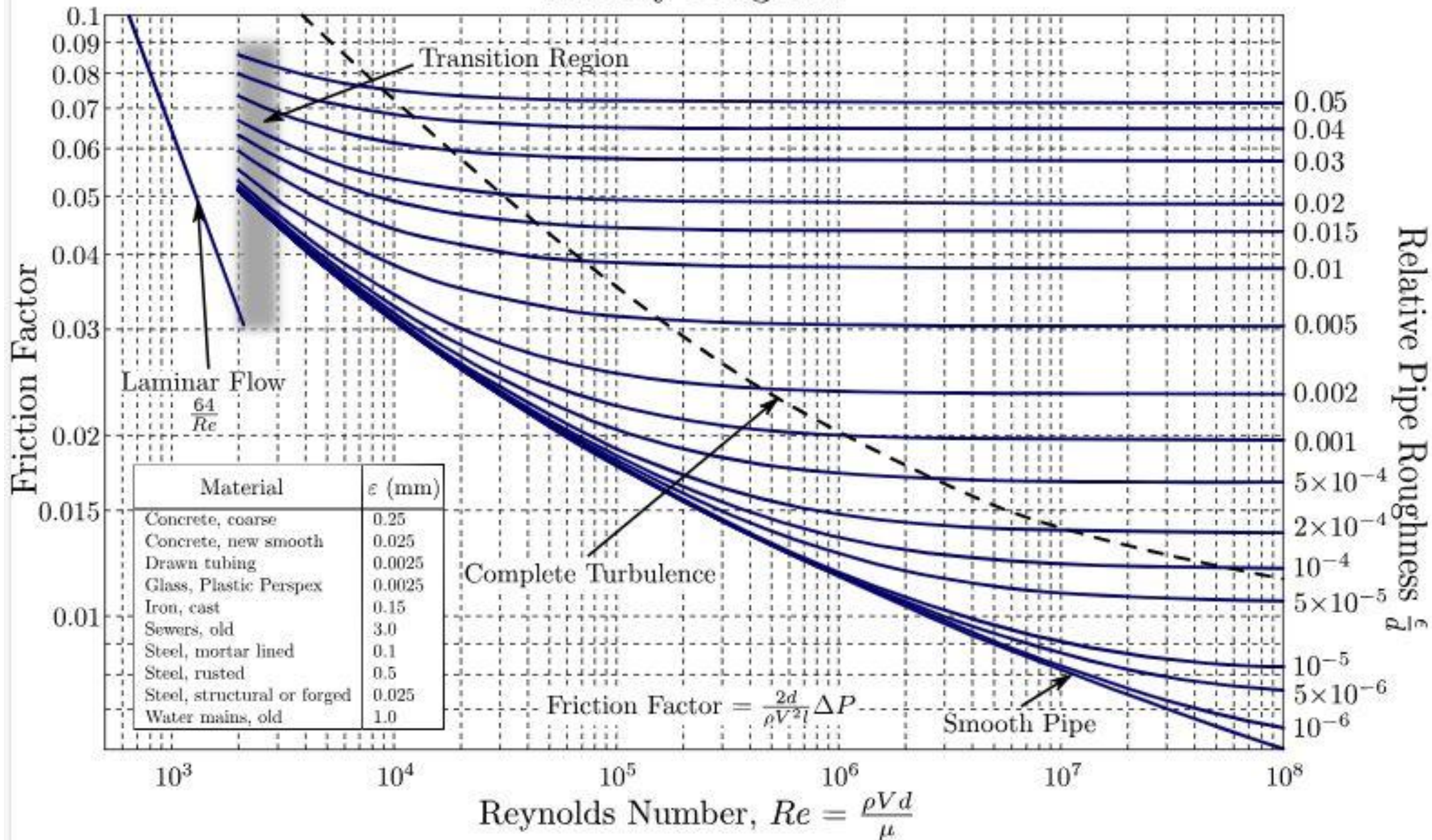
Velocity,  $V$  (m/s)

Major Loss,  $h_f$  (m)

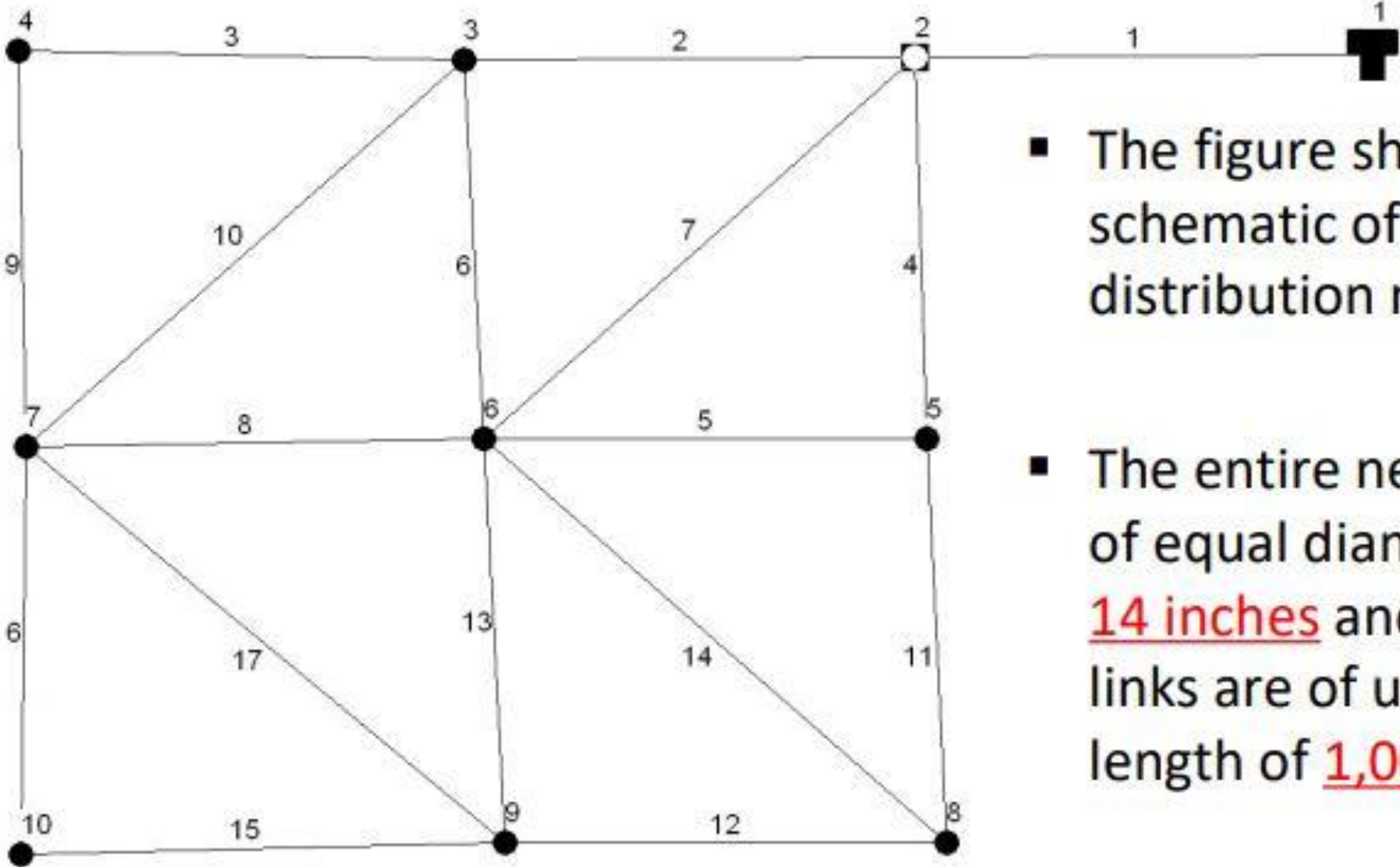
$g$  = acceleration due to gravity =  $9.806 \text{ m/s}^2$ .

The Darcy-Weisbach method is generally considered more accurate than the [Hazen-Williams method](#). Additionally, the Darcy-Weisbach method is valid for any liquid or gas; Hazen-Williams is only valid for water at ordinary temperatures (40 to 75 °F). The Hazen-Williams method is very popular, especially among civil engineers, since its friction coefficient ( $C$ ) is not a function of velocity or duct diameter. Hazen-Williams is simpler than Darcy-Weisbach for calculations where you are solving for flowrate, velocity, or diameter. More [Discussion and References](#).

# Moody Diagram



# Example 3



- The figure shows a schematic of a water distribution network
- The entire network is of equal diameters of 14 inches and the links are of uniform length of 1,000 m



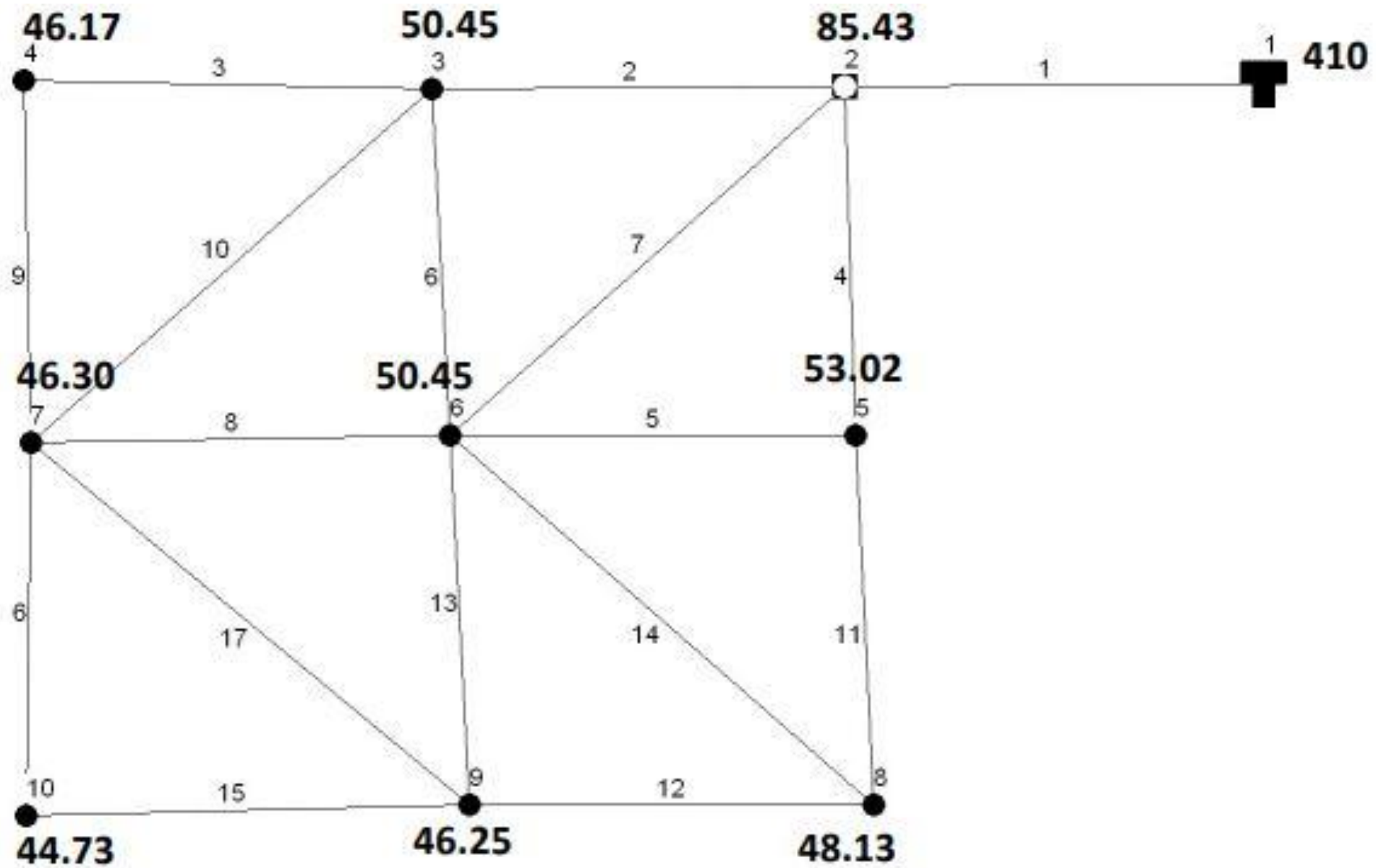
A hydraulic analysis was carried out for this network and the results of the pressure head and the total head at each node are summarized in the table

The pipes are at least 15 years old



| Node ID | Head<br>m | Pressure<br>m |
|---------|-----------|---------------|
| Junc 2  | 85.43     | 85.43         |
| Junc 3  | 50.45     | 50.45         |
| Junc 4  | 46.17     | 46.17         |
| Junc 5  | 53.02     | 53.02         |
| Junc 6  | 50.45     | 50.45         |
| Junc 7  | 46.30     | 46.30         |
| Junc 8  | 48.13     | 48.13         |
| Junc 9  | 46.25     | 46.25         |
| Junc 10 | 44.73     | 44.73         |
| Tank 1  | 410.00    | 10.00         |

- [1] Determine the direction of flow in links 8, 13, 15, 16, and 17
- [2] What is the net total water supply at node 6?
- [3] Where is the maximum link flow in the network and why?
- [4] What is the velocity in link 17?



[1] The main premise here is that water flows from the node of the higher total head to the node of lower total head. As such, link 8 (6→7), link 13 (6→9), link 15 (9→10), link 16 (7→10), and link 17 (7→9)

[2] We know that

$$h_f = 162.5 \left( \frac{Q}{C_{HW}} \right)^{1.852} D^{-4.87} L \rightarrow Q = \left( \frac{h_f}{162.5 \times D^{-4.87} L} \right)^{1/1.852} C_{HW}$$

We determine for each link connected to node 6 the headloss value and then from the above equation we can find out the flow. What you need to assume is the value of Hazen-Williams coefficient which was taken here as 100. As such, the following table was prepared:

|             | m                   | m                 | m                       | m <sup>3</sup> /h | m <sup>3</sup> /h |
|-------------|---------------------|-------------------|-------------------------|-------------------|-------------------|
| <b>Link</b> | <b>Initial head</b> | <b>Final head</b> | <b><math>h_f</math></b> | <b>Q</b>          | <b>Flow</b>       |
| 5           | 53.02               | 50.45             | 2.57                    | 263.97            | 263.97            |
| 6           | 50.45               | 50.45             | 0                       | 0                 | 0                 |
| 7           | 85.43               | 50.45             | 34.98                   | 1,080.95          | 1,080.95          |
| 8           | 50.45               | 46.3              | 4.15                    | 341.92            | -341.92           |
| 13          | 50.45               | 46.25             | 4.2                     | 344.14            | -344.14           |
| 14          | 50.45               | 48.13             | 2.32                    | 249.78            | -249.78           |
|             |                     |                   |                         | <b>Total</b>      | <b>409.08</b>     |

[3] The maximum flow is in link 1 because all the water to the nodes comes from the tank and thus the maximum flow is the total flow supplied by the network. The maximum must come at first from the tank through link 1

[4] The flow through the link is  $31.45 \text{ m}^3/\text{hr}$ . This gives a velocity of  $316.67 \text{ m/h}$